2.38 CFC-115(R115)

All equations for CFC-115(R115) are based on the Table from Thermophysical properties of refrigerants by Platzer *et al.*[1].

2.38.1 Temperature Scale

International practical temperature scale 1968 (IPTS-1968)

2.38.2 The Names of Substance, Library File and Single Shot Program

Name of Substance:	CFC-115, R115, Refrigerant 115, Freon 115, Chlorofluoroethane
Library File for UNIX:	libjr115.a
Library File for DOS,Windows95/NT:	JR115.LIB
Single Shot Program for UNIX:	r115-ss
Single Shot Program for DOS,Windows95/NT:	R115-SS.EXE

2.38.3 Important Constants and Others

Molecular Formula:	$C_2C\ell F_5$
Relative Molecular Mass:	154.480
Gas Constant:	53.997 J/(kg·K)

Critical Constants:

Critical Pressure:	3.1600×10^{6}Pa (31.600 bar)
Critical Temperature:	353.10 K (79.95 °C)
Critical Specific Volume:	1.6300×10^{-3}m^3/kg

Reference State:

At 0°C, 1.0000 kJ/(kg·K) and 200.00 kJ/kg are assigned to the specific entropy and the specific enthalpy of saturated liquid, respectively.

2.38.4 Formula

Equation of State:

The Bender equation of state (II·3·1) in reference [1], which is in a function from of $Z = Z(\rho, T)$. Here Z= compressibility, ρ=density and T=temperature.

Vapor Pressure:

Equation (20) in reference [1].

Properties at Vapor-Liquid Equilibrium:

saturated state: The Bender equation of state is utilized to obtaining saturated specific volume by the aid of Maxwell's criterion according to the author's recommendation. The Bender equation of state shows unreasonable behavior near the critical point. This temperature range is evaluated by $T_c \pm 1$ K. Therefore, in the temperature range and above the critical pressure, the values of u, h and s would include some uncertainity. Also, in the ranges of $p_{sat}(T_c - 1\text{K}) < p < p_{sat}(T_c + 1\text{K})$ and $v'(T_c - 1\text{K}) < v < v''(T_c - 1\text{K})$, the calculated values of p, v, T, c_p, c_v, isentropic exponent, Laplace coefficient, Prandtl number, velocity of sound and dryness fraction of wet vapor would have some uncertainity. Equations (2), (3), and (5) for specific enthalpy, specific entropy and isobaric specific heat, respectively. However, the sign of the last integration term in Equation (2) for u

$$u(T,\rho) = h_0 - RT_0 + \int_{T_0}^{T} (c_p^0 - R)dT + \int_0^{\rho} \left[T\left(\frac{\partial p}{\partial T}\right)_{\rho} - p \right] \frac{d\rho}{\rho^2}$$

has been corrected to

$$u(T,\rho) = h_0 - RT_0 + \int_{T_0}^{T} (c_p^0 - R)dT - \int_0^{\rho} \left[T\left(\frac{\partial p}{\partial T}\right)_{\rho} - p \right] \frac{d\rho}{\rho^2}.$$

However, the coefficients of Bender equation of state ($a_{01} \sim a_{19}$) are revised. The correct values are the followings.

$a_{01} = 2.3366423320E-02$
$a_{02} = 3.6254298340E+01$
$a_{03} = -8.9222216730E+03$
$a_{04} = 3.7757690770E+06$
$a_{05} = 2.3826225750E+08$
$a_{06} = 4.1067070490E-01$
$a_{07} = -2.6810832280E+02$
$a_{08} = 5.8910342990E+04$
$a_{09} = -4.1131369640E-01$
$a_{10} = 1.8247777160E+02$
$a_{11} = 4.5099307060E-01$
$a_{12} = -2.8676585670E+02$
$a_{13} = 7.2142477090E+01$
$a_{14} = -1.1555632860E+07$
$a_{15} = 4.3630653440E+09$
$a_{16} = -4.8300903530E+11$
$a_{17} = 1.7669793250E+07$
$a_{18} = -1.9335704800E+10$
$a_{19} = 3.8905495630E+12$

Transport Properties:
Thermal conductivity and viscosity from reference [2].

References

[1] B.Platzer, A.Polt and G.Maurer, Thermophysical Properties of Refrigerants (1990), Springer-Verlag
[2] Thermophysical Properties of Refrigerants(1976), 65 ASHRAE

Table II–2.38–1 CFC-115(R-115) Function

No.	Name of Function	Function and Argument(s)	Range of Argument(s)
1	AIPPT(P,T)		
94	AJTPT(P,T)		
8A	AKPD(P)		
8B	AKPDD(P)		
82	AKPT(P,T)	AKPT: Isentropic Exponent [–] P∗: Pressure [Pa], [bar] T∗: Temperature [K], [°C]	$30\times10^3\leq P\leq7.0\times10^6$ [Pa] $210\leq T\leq450$ [K] $0.3\leq P\leq70$ [bar] $-63.15\leq T\leq176.85$ [°C]
8C	AKTD(T)		
8D	AKTDD(T)		
2	ALAPP(P)		
3	ALAPT(T)		
4	ALHP(P)	ALHP: Latent Heat of Vaporization [J/kg] P∗: Pressure [Pa], [bar]	$16.25\times10^3\leq P\leq3.16\times10^6$ [Pa] $0.1625\leq P\leq31.6$ [bar]
5	ALHT(T)	ALHT: Latent Heat of Vaporization [J/kg] T∗: Temperature [K], [°C]	$200\leq T\leq353.1$ [K] $-73.15\leq T\leq79.95$ [°C]
6	ALMPD(P)	ALMPD: Thermal Conductivity of Saturated Liquid [W/(m·K)] P∗: Pressure [Pa], [bar]	$16.25\times10^3\leq P\leq0.9569\times10^6$ [Pa] $0.1625\leq P\leq9.569$ [bar]
7	ALMPDD(P)		
8	ALMPT(P,T)	ALMPT: Thermal Conductivity at Ordinary Pressure [W/(m·K)] P∗: Pressure [Pa], [bar] T∗: Temperature [K], [°C]	P=Dummy $240\leq T\leq380$ [K] $-33.15\leq T\leq106.85$ [°C]
9	ALMTD(T)	ALMTD: Thermal Conductivity of Saturated Liquid [W/(m·K)] T∗: Temperature [K], [°C]	$176\leq T\leq300$ [K] $-97.15\leq T\leq26.85$ [°C]
10	ALMTDD(T)		
11	AMUPD(P)	AMUPD: Coefficient of Viscosity of Saturated Liquid [Pa·s] P∗: Pressure [Pa], [bar]	$16.25\times10^3\leq P\leq0.7306\times10^6$ [Pa] $0.1625\leq P\leq7.306$ [bar]
12	AMUPDD(P)	AMUPDD: Coefficient of Viscosity of Saturated Vapor [Pa·s] P∗: Pressure [Pa], [bar]	$84.26\times10^3\leq P\leq2.9365\times10^6$ [Pa] $0.8426\leq P\leq29.635$ [bar]
13	AMUPT(P,T)		
14	AMUTD(T)	AMUTD: Coefficient of Viscosity of Saturated Liquid [Pa·s] T∗: Temperature [K], [°C]	$190\leq T\leq290$ [K] $-83.15\leq T\leq16.85$ [°C]
15	AMUTDD(T)	AMUTDD: Coefficient of Viscosity of Saturated Vapor [Pa·s] T∗: Temperature [K], [°C]	$230\leq T\leq350$ [K] $-43.15\leq T\leq76.85$ [°C]
92	BPPT(P,T)		
90	BSPT(P,T)		
91	BTPT(P,T)		
93	BVPT(P,T)		
16	CPPD(P)	CPPD: Isobaric Specific Heat of Saturated Liquid [J/(kg·K)] P∗: Pressure [Pa], [bar]	$16.25\times10^3\leq P\leq3.16\times10^6$ [Pa] $0.1625\leq P\leq31.6$ [bar]
17	CPPDD(P)	CPPDD: Isobaric Specific Heat of Saturated Vapor [J/(kg·K)] P∗: Pressure [Pa], [bar]	$16.25\times10^3\leq P\leq3.16\times10^6$ [Pa] $0.1625\leq P\leq31.6$ [bar]

Table II–2.38–1 CFC-115(R-115) Function (cont'd)

No.	Name of Function	Function and Argument(s)	Range of Argument(s)
18	CPPT(P,T)	CPPT: Isobaric Specific Heat [J/(kg·K)] P∗: Pressure [Pa], [bar] T∗: Temperature [K], [°C]	$30\times10^3 \le P \le 7.0\times10^6$ [Pa] $210 \le T \le 450$ [K] $0.3 \le P \le 70$ [bar] $-63.15 \le T \le 176.85$ [°C]
19	CPTD(T)	CPTD: Isobaric Specific Heat of Saturated Liquid [J/(kg·K)] T∗: Temperature [K], [°C]	$200 \le T \le 353.1$ [K] $-73.15 \le T \le 79.95$ [°C]
20	CPTDD(T)	CPTDD: Isobaric Specific Heat of Saturated Vapor [J/(kg·K)] T∗: Temperature [K], [°C]	$200 \le T \le 353.1$ [K] $-73.15 \le T \le 79.95$ [°C]
21	CRP('A')	CRP: Critical Constants H: 'A'='H': 0.3125×10^6 [J/kg] Specific Enthalpy P∗: 'A'='P': 3.16×10^6 [Pa], 31.6 [bar] Pressure S: 'A'='S': 1.345×10^3 [J/(kg·K)] Specific Entropy T∗: 'A'='T': 353.10 [K], 79.95 [°C] Temperature V: 'A'='V': 1.630×10^{-3} [m^3/kg] Specific Volume	one of 'H', 'P', 'S', 'T' and 'V'
7A	CVPD(P)		
76	CVPDD(P)	CVPDD: Isochoric Specific Heat of Saturated Vapor [J/(kg·K)] P∗: Pressure [Pa], [bar]	$16.25\times10^3 \le P \le 3.16\times10^6$ [Pa] $0.1625 \le P \le 31.6$ [bar]
77	CVPT(P,T)	CVPT: Isochoric Specific Heat [J/(kg·K)] P∗: Pressure [Pa], [bar] T∗: Temperature [K], [°C]	$30\times10^3 \le P \le 7.0\times10^6$ [Pa] $210 \le T \le 450$ [K] $0.3 \le P \le 70$ [bar] $-63.15 \le T \le 176.85$ [°C]
7B	CVTD(T)		
78	CVTDD(T)	CVTDD: Isochoric Specific Heat of Saturated Vapor [J/(kg·K)] T∗: Temperature [K], [°C]	$200 \le T \le 353.1$ [K] $-73.15 \le T \le 79.95$ [°C]
2A	EPSPD(P)		
2B	EPSPDD(P)		
22	EPSPT(P,T)		
2C	EPSTD(T)		
2D	EPSTDD(T)		
89	FC('A')	FC: Fundamental Constants M: 'A'='M': 154.48 Relative Molecular Mass R: 'A'='R': 53.997 [J/(kg·K)] Gas Constant	one of 'M' and 'R'
9A	GAMPD(P)		
96	GAMPDD(P)		
95	GAMPT(P,T)		
9B	GAMTD(T)		
97	GAMTDD(T)		
23	HPD(P)	HPD: Specific Enthalpy of Saturated Liquid [J/kg] P∗: Pressure [Pa], [bar]	$16.25\times10^3 \le P \le 3.16\times10^6$ [Pa] $0.1625 \le P \le 31.6$ [bar]
24	HPDD(P)	HPDD: Specific Enthalpy of Saturated Vapor [J/kg] P∗: Pressure [Pa], [bar]	$16.25\times10^3 \le P \le 3.16\times10^6$ [Pa] $0.1625 \le P \le 31.6$ [bar]
71	HPS(P,S)	HPS: Specific Enthalpy [J/kg] P∗: Pressure [Pa], [bar] S: Specific Entropy [J/(kg·K)]	$30\times10^3 \le P \le 7.0\times10^6$ [Pa] $SPT(P,210K) \le S \le$ SPT(P,450K) [J/(kg·K)] $0.3 \le P \le 70$ [bar] $SPT(P,-63.15°C) \le S \le$ SPT(P,176.85°C) [J/(kg·K)]

Table II–2.38–1 CFC-115(R-115) Function (cont'd)

No.	Name of Function	Function and Argument(s)	Range of Argument(s)
25	HPT(P,T)	HPT: Specific Enthalpy [J/kg] P∗: Pressure [Pa], [bar] T∗: Temperature [K], [°C]	$30\times10^3\leq P\leq7.0\times10^6$ [Pa] $210\leq T\leq450$ [K] $0.3\leq P\leq70$ [bar] $-63.15\leq T\leq176.85$ [°C]
26	HPX(P,X)	HPX: Specific Enthalpy of Mixture [J/kg] P∗: Pressure [Pa], [bar] X: Dryness Fraction [–]	$16.25\times10^3\leq P\leq3.16\times10^6$ [Pa] $0.1625\leq P\leq31.6$ [bar] $0\leq X\leq1.0$ [–]
27	HTD(T)	HTD: Specific Enthalpy of Saturated Liquid [J/kg] T∗: Temperature [K], [°C]	$200\leq T\leq353.1$ [K] $-73.15\leq T\leq79.95$ [°C]
28	HTDD(T)	HTDD: Specific Enthalpy of Saturated Vapor [J/kg]	$200\leq T\leq353.1$ [K] $-73.15\leq T\leq79.95$ [°C]
29	HTX(T,X)	HTX: Specific Enthalpy of Mixture [J/kg] T∗: Temperature [K], [°C] X: Dryness Fraction [–]	$200\leq T\leq353.1$ [K] $-73.15\leq T\leq79.95$ [°C] $0\leq X\leq1.0$ [–]
84	IDENTF('A')	IDENTF: CHARACTER TYPE FUNCTION for Identification of Substance (Length 20) C: 'A'='C':'CCLF2CF3' Molecular Formula S: 'A'='S':'CFC-115(R-115)' Name of Substance V: 'A'='V':'10.1' Version Number	one of 'C', 'S' and 'V'
66	PLDT(T)		
68	PMLT(T)		
85	PRPD(P)	PRPD: Prandtl Number of Saturated Liquid [–] P∗: Pressure [Pa], [bar]	$16.25\times10^3\leq P\leq0.7306\times10^6$ [Pa] $0.1625\leq P\leq7.306$ [bar]
86	PRPDD(P)		
81	PRPT(P,T)		
87	PRTD(T)	PRTD: Prandtl Number of Saturated Liquid [–] T∗: Temperature [K], [°C]	$200\leq T\leq290$ [K] $-73.15\leq T\leq16.85$ [°C]
88	PRTDD(T)		
99	PSBT(T)		
30	PST(T)	PST∗: Saturation Pressure [Pa], [bar] T∗: Temperature [K], [°C]	$210\leq T\leq353.1$ [K] $-73.15\leq T\leq79.95$ [°C]
72	PSTD(T)		
73	PSTDD(T)		
31	SIGP(P)	SIGP: Surface Tension [N/m] P∗: Pressure [Pa], [bar]	PST(200K)$\leq P\leq3.16\times10^6$ [Pa] ($\sim20\times10^3$) PST(-73.15°C)$\leq P\leq31.6$ [bar] (~0.2)
32	SIGT(T)	SIGT: Surface Tension [N/m] T∗: Temperature [K], [°C]	$200\leq T\leq353.1$ [K] $-73.15\leq T\leq79.95$ [°C]
33	SPD(P)	SPD: Specific Entropy of Saturated Liquid [J/(kg·K)] P∗: Pressure [Pa], [bar]	$16.25\times10^3\leq P\leq3.16\times10^6$ [Pa] $0.1625\leq P\leq31.6$ [bar]
34	SPDD(P)	SPDD: Specific Entropy of Saturated Vapor [J/(kg·K)] P∗: Pressure [Pa], [bar]	$16.25\times10^3\leq P\leq3.16\times10^6$ [Pa] $0.1625\leq P\leq31.6$ [bar]
35	SPT(P,T)	SPT: Specific Entropy [J/(kg·K)] P∗: Pressure [Pa], [bar] T∗: Temperature [K], [°C]	$30\times10^3\leq P\leq7.0\times10^6$ [Pa] $210\leq T\leq450$ [K] $0.3\leq P\leq70$ [bar] $-63.15\leq T\leq176.85$ [°C]
36	SPX(P,X)	SPX: Specific Entropy of Mixture [J/(kg·K)] P∗: Pressure [Pa], [bar] X: Dryness Fraction [–]	$16.25\times10^3\leq P\leq3.16\times10^6$ [Pa] $0.1625\leq P\leq31.6$ [bar] $0\leq X\leq1.0$ [–]

Table II–2.38–1 CFC-115(R-115) Function (cont'd)

No.	Name of Function	Function and Argument(s)	Range of Argument(s)
37	STD(T)	STD: Specific Entropy of Saturated Liquid [J/(kg·K)] T∗: Temperature [K], [°C]	200≤T≤353.1 [K] −73.15≤T≤79.95 [°C]
38	STDD(T)	STDD: Specific Entropy of Saturated Vapor [J/(kg·K)] T∗: Temperature [K], [°C]	200≤T≤353.1 [K] −73.15≤T≤79.95 [°C]
39	STX(T,X)	STX: Specific Entropy of Mixture [J/(kg·K)] T∗: Temperature [K], [°C] X: Dryness Fraction [–]	200≤T≤353.1 [K] −73.15≤T≤79.95 [°C] 0≤X≤1.0 [–]
67	TLDP(P)		
69	TMLP(P)		
64	TPH(P,H)	TPH∗: Temperature [K], [°C] P∗: Pressure [Pa], [bar] H: Specific Enthalpy [J/kg]	30×10^3≤P≤7.0×10^6 [Pa] HPT(P,210K)≤H≤ HPT(P,450K) [J/kg] 0.3≤P≤70 [bar] HPT(P,−63.15°C)≤H≤ HPT(P,176.85°C) [J/kg]
6H	TPH2(P,H)		
65	TPS(P,S)	TPS∗: Temperature [K], [°C] P∗: Pressure [Pa], [bar] S: Specific Entropy [J/(kg·K)]	30×10^3≤P≤7.0×10^6 [Pa] SPT(P,210K)≤S≤ SPT(P,450K) [J/(kg·K)] 0.3≤P≤70 [bar] SPT(P,−63.15°C)≤S≤ SPT(P,176.85°C) [J/(kg·K)]
6S	TPS2(P,S)		
98	TPSEUP(P)		
70	TPV(P,V)	TPV∗: Temperature [K], [°C] P∗: Pressure [Pa], [bar] V: Specific Volume [m^3/kg]	30×10^3≤P≤7.0×10^6 [Pa] VPT(P,210K)≤V≤ VPT(P,450K) [m^3/kg] 0.3≤P≤70 [bar] VPT(P,−63.15°C)≤V≤ VPT(P,176.85°C) [m^3/kg]
41	TRPL('A')		
100	TSBP(P)		
40	TSP(P)	TSP∗: Saturation Temperature [K], [°C] P∗: Pressure [Pa], [bar]	16.25×10^3≤P≤3.16×10^6 [Pa] 0.1625≤P≤31.6 [bar]
74	TSPD(P)		
75	TSPDD(P)		
42	UPD(P)	UPD: Specific Internal Energy of Saturated Liquid [J/kg] P∗: Pressure [Pa], [bar]	16.25×10^3≤P≤3.16×10^6 [Pa] 0.1625≤P≤31.6 [bar]
43	UPDD(P)	UPDD: Specific Internal Energy of Saturated Vapor [J/kg] P∗: Pressure [Pa], [bar]	16.25×10^3≤P≤3.16×10^6 [Pa] 0.1625≤P≤31.6 [bar]
79	UPS(P,S)	UPS: Specific Internal Energy [J/kg] P∗: Pressure [Pa], [bar] S: Specific Entropy [J/(kg·K)]	16.25×10^3≤P≤10.0×10^6 [Pa] SPT(P,210K)≤S≤ SPT(P,450K) [J/(kg·K)] 0.3≤P≤70 [bar] SPT(P,−63.15°C)≤S≤ SPT(P,176.85°C) [J/(kg·K)]
44	UPT(P,T)	UPT: Specific Internal Energy [J/kg] P∗: Pressure [Pa], [bar] T∗: Temperature [K], [°C]	30×10^3≤P≤7.0×10^6 [Pa] 210≤T≤450 [K] 0.3≤P≤70 [bar] −63.15≤T≤176.85 [°C]

Table II–2.38–1 CFC-115(R-115) Function (cont'd)

No.	Name of Function	Function and Argument(s)	Range of Argument(s)
45	UPX(P,X)	UPX: Specific Internal Energy of Mixture [J/kg] P∗: Pressure [Pa], [bar] X: Dryness Fraction [–]	$16.25\times10^3\leq P\leq3.16\times10^6$ [Pa] $0.1625\leq P\leq31.6$ [bar] $0\leq X\leq1.0$ [–]
46	UTD(T)	UTD: Specific Internal Energy of Saturated Liquid [J/kg] T∗: Temperature [K], [°C]	$200\leq T\leq353.1$ [K] $-73.15\leq T\leq79.95$ [°C]
47	UTDD(T)	UTDD: Specific Internal Energy of Saturated Vapor [J/kg] T∗: Temperature [K], [°C]	$200\leq T\leq353.1$ [K] $-73.15\leq T\leq79.95$ [°C]
48	UTX(T,X)	UTX: Specific Internal Energy of Mixture [J/kg] T∗: Temperature [K], [°C] X: Dryness Fraction [–]	$200\leq T\leq353.1$ [K] $-73.15\leq T\leq79.95$ [°C] $0\leq X\leq1.0$ [–]
49	VPD(P)	VPD: Specific Volume of Saturated Liquid [m^3/kg] P∗: Pressure [Pa], [bar]	$16.25\times10^3\leq P\leq3.16\times10^6$ [Pa] $0.1625\leq P\leq31.6$ [bar]
50	VPDD(P)	VPDD: Specific Volume of Saturated Vapor [m^3/kg] P∗: Pressure [Pa], [bar]	$16.25\times10^3\leq P\leq3.16\times10^6$ [Pa] $0.1625\leq P\leq31.6$ [bar]
80	VPS(P,S)	VPS: Specific Volume [m^3/kg] P∗: Pressure [Pa], [bar] S: Specific Entropy [J/(kg·K)]	$30\times10^3\leq P\leq7.0\times10^6$ [Pa] SPT(P,210K)≤S≤ SPT(P,450K) [J/(kg·K)] $0.3\leq P\leq70$ [bar] SPT(P,−63.15°C)≤S≤ SPT(P,176.85°C) [J/(kg·K)]
51	VPT(P,T)	VPT: Specific Volume [m^3/kg] P∗: Pressure [Pa], [bar] T∗: Temperature [K], [°C]	$30\times10^3\leq P\leq7.0\times10^6$ [Pa] $210\leq T\leq450$ [K] $0.3\leq P\leq70$ [bar] $-63.15\leq T\leq176.85$ [°C]
52	VPX(P,X)	VPX: Specific Volume of Mixture [m^3/kg] P∗: Pressure [Pa], [bar] X: Dryness Fraction [–]	$16.25\times10^3\leq P\leq3.16\times10^6$ [Pa] $0.1625\leq P\leq31.6$ [bar] $0\leq X\leq1.0$ [–]
53	VTD(T)	VTD: Specific Volume of Saturated Liquid [m^3/kg] T∗: Temperature [K], [°C]	$200\leq T\leq353.1$ [K] $-73.15\leq T\leq79.95$ [°C]
54	VTDD(T)	VTDD: Specific Volume of Saturated Vapor [m^3/kg] T∗: Temperature [K], [°C]	$200\leq T\leq353.1$ [K] $-73.15\leq T\leq79.95$ [°C]
55	VTX(T,X)	VTX: Specific Volume of Mixture [m^3/kg] T∗: Temperature [K], [°C] X: Dryness Fraction [–]	$200\leq T\leq353.1$ [K] $-73.15\leq T\leq79.95$ [°C] $0\leq X\leq1.0$ [–]
8E	WPD(P)		
8F	WPDD(P)		
83	WPT(P,T)	WPT: Velocity of Sound [m/s] P∗: Pressure [Pa], [bar] T∗: Temperature [K], [°C]	$30\times10^3\leq P\leq7.0\times10^6$ [Pa] $210\leq T\leq450$ [K] $0.3\leq P\leq70$ [bar] $-63.15\leq T\leq176.85$ [°C]
8G	WTD(T)		
8H	WTDD(T)		
56	XPH(P,H)	XPH: Dryness Fraction [–] P∗: Pressure [Pa], [bar] H: Specific Enthalpy of Mixture [J/kg]	$16.25\times10^3\leq P<3.16\times10^6$ [Pa] $0.1625\leq P<31.6$ [bar] HPD(P)≤H≤HPDD(P) [J/kg]
57	XPS(P,S)	XPS: Dryness Fraction [–] P∗: Pressure [Pa], [bar] S: Specific Entropy of Mixture [J/(kg·K)]	$16.25\times10^3\leq P<3.16\times10^6$ [Pa] $0.1625\leq P<31.6$ [bar] SPD(P)≤S≤SPDD(P) [J/(kg·K)]

Table II–2.38–1 CFC-115(R-115) Function (cont'd)

No.	Name of Function	Function and Argument(s)	Range of Argument(s)
58	XPU(P,U)	XPU: Dryness Fraction [–] P∗: Pressure [Pa], [bar] U: Specific Internal Energy of Mixture [J/kg]	$16.25\times10^3\leq$P$<3.16\times10^6$ [Pa] $0.1625\leq$P<31.6 [bar] UPD(P)$\leq$U$\leq$UPDD(P) [J/kg]
59	XPV(P,V)	XPV: Dryness Fraction [–] P∗: Pressure [Pa], [bar] V: Specific Volume of Mixture [m^3/kg]	$16.25\times10^3\leq$P$<3.16\times10^6$ [Pa] $0.1625\leq$P<31.6 [bar] VPD(P)$\leq$V$\leq$VPDD(P) [m^3/kg]
60	XTH(T,H)	XTH: Dryness Fraction [–] T∗: Temperature [K], [°C] H: Specific Enthalpy of Mixture [J/kg]	$200\leq$T<353.1 [K] $-73.15\leq$T<79.95 [°C] HTD(T)$\leq$H$\leq$HTDD(T) [J/kg]
61	XTS(T,S)	XTS: Dryness Fraction [–] T∗: Temperature [K], [°C] S: Specific Entropy of Mixture [J/(kg·K)]	$200\leq$T<353.1 [K] $-73.15\leq$T<79.95 [°C] STD(T)$\leq$S$\leq$STDD(T) [J/(kg·K)]
62	XTU(T,U)	XTU: Dryness Fraction [–] T∗: Temperature [K], [°C] U: Specific Internal Energy of Mixture [J/kg]	$200\leq$T<353.1 [K] $-73.15\leq$T<79.95 [°C] UTD(T)$\leq$U$\leq$UTDD(T) [J/kg]
63	XTV(T,V)	XTV: Dryness Fraction [–] T∗: Temperature [K], [°C] V: Specific Volume of Mixture [m^3/kg]	$200\leq$T<353.1 [K] $-73.15\leq$T<79.95 [°C] VTD(T)$\leq$V$\leq$VTDD(T) [m^3/kg]